

AMENDMENTS TO THE CLAIMS

We claim:

1. (Currently Amended) A process for preparing mono- or diesters of polytetrahydrofuran or of tetrahydrofuran copolymers by comprising polymerizing tetrahydrofuran in the presence of at least one telogen and/or of a comonomer over an acidic catalyst, wherein the polymerization reactor is started up using a mixture of the polymer to be prepared by the process, polytetrahydrofuran, the mono- or diesters of polytetrahydrofuran and/or of the tetrahydrofuran copolymers, tetrahydrofuran, any comonomer and at least one carboxylic anhydride.
2. (Currently Amended) ~~A process as claimed in claim 1~~ The process according to claim 1, wherein the mono- or diesters of polytetrahydrofuran or of the tetrahydrofuran copolymers or the polytetrahydrofuran used for startup have an average molecular weight M_n of from 650 to 4000.
3. (Currently Amended) ~~A process as claimed in claim 1 or 2~~ The process according to claim 1, wherein the concentration of the polymer used for startup is from 20 to 80% by weight, based on the total amount of the mixture used for startup.
4. (Currently Amended) ~~A process as claimed in any of claims 1 to 3~~ The process according to claim 1, wherein the mixture used for startup comprises from 7 to 80% by weight of tetrahydrofuran or the total amount of tetrahydrofuran and comonomer, based on the total amount of the mixture used for startup.
5. (Currently Amended) ~~A process as claimed in any of claims 1 to 4~~ The process according to claim 1, wherein from 0.5 to 10% by weight of carboxylic anhydride are used for startup, based on the entire amount of the mixture used for startup.

6. (Currently Amended) ~~A process as claimed in any of claims 1 to 5~~ The process according to claim 1, wherein acetic anhydride is used.
7. (Currently Amended) ~~A process as claimed in any of claims 1 to 6~~ The process according to claim 1, wherein, in addition to the carboxylic anhydride, up to 3% by weight, based on the total amount of the mixture used for startup, of carboxylic acid are used.
8. (Currently Amended) ~~A process as claimed in any of claims 1 to 7~~ The process according to claim 1, wherein an inert solvent is added to the mixture used for starting up the polymerization reactor.
9. (New) The process according to claim 2, wherein the concentration of the polymer used for startup is from 20 to 80% by weight, based on the total amount of the mixture used for startup.
10. (New) The process according to claim 2, wherein the mixture used for startup comprises from 7 to 80% by weight of tetrahydrofuran or the total amount of tetrahydrofuran and comonomer, based on the total amount of the mixture used for startup.
11. (New) The process according to claim 3, wherein the mixture used for startup comprises from 7 to 80% by weight of tetrahydrofuran or the total amount of tetrahydrofuran and comonomer, based on the total amount of the mixture used for startup.
12. (New) The process according to claim 2, wherein from 0.5 to 10% by weight of carboxylic anhydride are used for startup, based on the entire amount of the mixture used for startup.
13. (New) The process according to claim 3, wherein from 0.5 to 10% by weight of carboxylic anhydride are used for startup, based on the entire amount of the mixture used for startup.

14. (New) The process according to claim 4, wherein from 0.5 to 10% by weight of carboxylic anhydride are used for startup, based on the entire amount of the mixture used for startup.

15. (New) The process according to claim 2, wherein acetic anhydride is used.

16. (New) The process according to claim 3, wherein acetic anhydride is used.

17. (New) The process according to claim 4, wherein acetic anhydride is used.

18. (New) The process according to claim 5, wherein acetic anhydride is used.

19. (New) The process according to claim 2, wherein, in addition to the carboxylic anhydride, up to 3% by weight, based on the total amount of the mixture used for startup, of carboxylic acid are used.

20. (New) The process according to claim 3, wherein, in addition to the carboxylic anhydride, up to 3% by weight, based on the total amount of the mixture used for startup, of carboxylic acid are used.